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**10ME63** 

 $(06 Marks)$ 

 $(06 Marks)$ 

## Sixth Semester B.E. Degree Examination, July/August 2021 **Heat and Mass Transfer**

Max. Marks:100

## Time: 3 hrs.

 $\mathbf{1}$ 

 $\overline{2}$ 

3

## Note: 1. Answer any FIVE full questions. 2. Use Heat and Mass transfer Data Hand Book is permitted. 3. Assume missing data if any.

- Write basic laws governing each mode of heat transfer along with mathematical expressions. a.
- $\mathbf{b}$ . Write boundary conditions of first, second and third kinds
- Consider a slab of thickness L. A fluid at a temperature 130°C with a heat transfer c. coefficient 250 W/m<sup>2</sup>°C flows over the surface at  $x = 0$ , and another fluid at a temperature 30°C, with a heat transfer coefficient 500 W/m<sup>2</sup>°C flows over the surface at  $x = L$  of the plate. Assuming K for the slab 20 W/m<sup>o</sup>C, calculate the heat flow rate per  $m<sup>2</sup>$  of slab if the slab thickness is 4 cm. Determine the slab thickness if the heat flow rate is to be reduced to  $(08 Marks)$ 50%.
- Derive an expression for the temperature distribution  $T(x)$  and for heat flow through an area a. A of the slab of thickness L. Boundary conditions are at  $x = 0$ ,  $T = T_1$  and at  $x = L$ ,  $T = T_2$ . There is no energy generation in the solid and thermal conductivity is constant.  $(10 Marks)$  $(04 Marks)$ 
	- Explain (i) Critical thickness of insulation (ii) fin efficiency.  $b<sub>1</sub>$
	- A steel rod of diameter 2 cm, length 20 cm and thermal conductivity  $K = 50$  W/m<sup>°</sup>C is  $\mathbf{c}$ . exposed to ambient air at 20°C with a heat transfer coefficient 64 W/m<sup>2°</sup>C. If one end of the rod is at a temperature 115°C, calculate the heat loss from the rod. Assume long fin.

 $(06 Marks)$ 

- Explain the significance of.  $a<sub>1</sub>$ 
	- (i) Biot number (ii) Fourier number. (iii) Heisler charts.  $(06 Marks)$
	- Explain the criteria for neglecting internal temperature gradients.  $(04 Marks)$  $\mathbf b$ .
	- The temperature of a gas stream is measured with a thermocouple. Junction may be  $\mathbf{c}$ . approximated as a sphere of diameter D = 2 mm, with K = 30 W/m<sup>°</sup>C,  $\rho = 8600 \text{ kg/m}^3$ ,  $C_p = 400$  J/kg<sup>°</sup>C. The heat transfer coefficient is  $h = 280$  W/m<sup>2°</sup>C. How long will it take for the thermocouple to record 98 percent of the applied temperature difference?  $(10 Marks)$
- Sketch and explain in brief each of the following:  $\overline{\mathbf{4}}$ 
	- Velocity boundary layer for flow along a flat plate.  $(i)$
	- Thermal boundary layer for flow of a hot fluid over a cold wall.  $(ii)$
	- (iii) Hydrodynamic entry region and hydrodynamically developed region.  $(12 Marks)$ b. A square plate 0.4 by 0.4 m maintained at a uniform temperature of  $T_w = 400$  K is suspended vertically in quiescent atmospheric air at  $T_{\infty}$  = 300 K.
		- Determine the boundary layer thickness  $\delta(x)$  at the trailing edge of the plate  $(i)$  $(at x = 0.4 m)$
		- Calculate the average heat transfer coefficient h over the entire length of the plate by  $(ii)$ using the relations given below:

Properties of air at 350 K

$$
\gamma = 20.75 \times 10^{-6} \text{ m}^2\text{/s}, \ P_r = 0.697, \ K = 0.03 \text{ W/m}^{\circ}\text{C}
$$
  
\n
$$
\delta(x)|_{x=1} = 3.93 \text{ P}_r^{-\frac{1}{2}}(0.952 + \text{P}_r)^{\frac{1}{4}}\text{G}_r^{-\frac{1}{4}}\text{L}, \ \text{NU}_m = 0.518(\text{Gr}_L\text{P}_r)^{\frac{1}{4}}.
$$
 (08 Marks)  
\n1 of 2

 $(04 Marks)$ 

 $(08 Marks)$ 

What is the physical significance of, 5  $a<sub>1</sub>$ 

 $(i)$ 

 $(vii)$ 

- Reynolds number.  $(ii)$ Prandtl number.  $(i)$
- The convection heat transfer coefficients for flow of a fluid through a tube have been  $b.$ experimentally determined. Using dimensional analysis obtain the relationship  $Nu = f(Re \cdot Pr)$

The following physical quantities may be assumed to influence convection :

 $(vi)$ 

- (ii) Thermal conductivity, K Tube diameter, D.
- $(ii)$ Velocity, u
- (iv) Density  $\rho$ .
- $(v)$ Viscosity, µ

Heat transfer coefficient, h

Specific heat, C<sub>p</sub> and

- c. Water flows with a mean velocity of  $U_m = 2$  m/s inside a circular pipe of inside diameter
	- D = 5 cm. Assume the pipe is smooth and maintained at uniform temperature  $T_w = 100^{\circ}C$  by condensing steam on its outer surface. At a location where the fluid is hydrodynamically and thermally developed, the bulk mean temperature of water is  $60^{\circ}$ C. Calculate the heat transfer coefficient h using (i) Dittus and Boelter equation (ii) Sieder-Tate equation. Take properties at 60°C (mean T)

K = 0.651 W/m<sup>o</sup>C, P<sub>r</sub> = 3.02, p = 985 kg/m<sup>3</sup>,  $\mu_m = 4.71 \times 10^{-4}$  kg/m.s (at mean T),  $\mu_w = 2.82 \times 10^{-4}$  kg/m.s (at wall T)

(i) Dittus-Boelter equation is  $Nu = 0.023R_e^{0.8}P_r^{n}$ , n = 0.4 for heating and 0.3 for cooling.

(ii) Sieder-Tate equation is, Nu = 0.027
$$
R_e^{0.8}P_r^{\frac{1}{3}}\left(\frac{\mu_m}{\mu_w}\right)^{0.14}
$$
. (08 Marks)

How are heat exchangers classified? 6  $a<sub>1</sub>$ 

- What is fouling? List the factors that cause fouling.  $(04 Marks)$  $\mathbf b$ .
- c. A counter flow heat exchanger of heat transfer area  $A = 12.5 m^2$  is to cool oil [C<sub>ph</sub> = 2000 J/kg.S] with water [C<sub>PC</sub> = 4170 J/kg.S]. The oil enters at T<sub>hi</sub> = 100°C and m<sub>h</sub> = 2 kg/s, while the water enters at T<sub>Ci</sub> = 20°C and m<sub>C</sub> = 0.48 kg/s. The overall heat transfer coefficient is  $U_m = 400 \text{ W/m}^2$ °C. Calculate the exit temperature of water and the total heat transfer rate Q.  $(10 Marks)$
- Explain types of condensation.  $\overline{7}$  $a<sub>1</sub>$ 
	- Sketch and explain regimes of pool boiling.  $\mathbf{b}$ .
	- A vertical square plate 30 by 30 cm, is exposed to steam at atmospheric pressure. The plate c. temperature is 98°C. Calculate the heat transfer and the mass of steam condensed per hour. What is the nature of flow?

Use the properties given below at 99°C

$$
\rho_f = 960 \text{ kg/m}^3, \ \mu_f = 2.82 \times 10^{-4} \text{ kg/m.s}, \ \text{K}_f = 0.68 \text{ W/m}^{\circ} \text{C}, \ \text{T}_{\text{sat}} = 100^{\circ} \text{C}, \ \text{h}_{\text{fg}} = 2255 \text{ KJ/kg}.
$$
\n(10 Marks)

Define the following with mathematical expressions: 8

- (ii) Hemispherical emissivity. Spectral hemispherical emissivity.  $(i)$
- Spectral Black body emissive power. (iv)Blackbody emissive power. (08 Marks)  $(iii)$
- Explain concept of view factor and its physical significance.  $\mathbf{b}$ .  $(04 Marks)$
- The emission of radiation from a surface can be approximated as a black body radiation at  $\mathbf{C}$ .  $T = 1000$  K.
	- What fraction of the total energy emitted is below  $\lambda = 5 \mu m$ ?  $(i)$
	- What is the wave length below which the emission is 10.5 % of the total emission at  $(ii)$ 1000 K?
	- (iii) What is the wavelength at which the maximum spectral emission occurs at  $T=1000$  K?  $(08 Marks)$

## $(04 Marks)$

 $(06 Marks)$ 

 $(06 Marks)$